

THERMODYNAMIC CHART  
FOR THE COMBUSTION  
PROCESS IN DIESEL CYCLES

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WILLIAN F. FARRELL, JR.

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FOR THE COMBUSTION PROCESS  
IN DIESEL CYCLES

by

William F. Farrell, Jr.,  
Lieutenant Commander, United States Navy

Submitted in partial fulfillment  
of the requirements  
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## PREFACE

A number of thermodynamic charts for internal combustion processes have been prepared in the last twenty years. None of those presently available, however, cover the pressure, temperature and fuel-air ratios of diesel cycles.

The purpose of this project is the preparation of one thermodynamic chart of a typical diesel fuel-air ratio, covering the usual temperature and pressure ranges encountered in the combustion portion of the diesel cycle. The work was undertaken at the suggestion of the Internal Combustion Engine Division of the Bureau of Ships, which furnished the author with the necessary data on pressure and temperature range, and fuel-air ratio.

During the period from November, 1950 through May 1951, the author made the analysis and computations necessary for the project and constructed the thermodynamic chart. Investigation was further made toward a simplified method of attack for the problem of construction of the low pressure-low temperature region of this chart for determination of the thermodynamic properties of the combustion products in the remainder of the diesel cycle, i.e., the adiabatic reversible expansion, and the opening of the exhaust valve and release of pressure to atmospheric.

The author gratefully acknowledges the timely assistance, advice and guidance of Professor Gilbert F. Kinney of the Department of Chemistry and Metallurgy of the U. S. Naval Postgraduate School throughout the entire project. Acknow-



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The entire project was conducted at the United States Naval Postgraduate School.





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## LIST OF SYMBOLS

$P$	Pressure (total), in atmospheres
$P_i$	Pressure (partial), in atmospheres
$p$	Pressure (total), lbs./sq. in.
$T$	Temperature, $^{\circ}$ Rankine
$V$	Volume, cubic feet
$E$	Internal Energy, B.T.U., above $\text{CO}_2$ , $\text{H}_2\text{O}$ (vapor), $\text{O}_2$ and air- $\text{N}_2$ at $100^{\circ}$ F
$E_s$	Sensible Internal Energy, $(E - Q_v)$ , in B.T.U.
$Q_v$	Internal Energy of Combustion, at $100^{\circ}$ F, of unburned fuel in equilibrium mixture at temperature $T$ , in B.T.U.
$H$	Enthalpy, B.T.U., $E - J(pV)$
$S$	Entropy, B.T.U./ $^{\circ}$ Rankine, above $\text{CO}_2$ , $\text{H}_2\text{O}$ (vapor), $\text{O}_2$ and air- $\text{N}_2$ , each at one atmosphere and $100^{\circ}$ F
$R$	Universal gas constant
$J$	Conversion factor, 1 B.T.U. = 778 ft. lbs.
$k$	Mean Specific Heat Ratio
$K_i$ - $K_c$	Equilibrium constants
$x_i$	Mole fraction of each chemical species at equilibrium
$m$	Moles of each chemical species at equilibrium
$\sum m$	Total moles of combustion products



## CHAPTER I

### INTRODUCTION

The large fraction of combustion processes of interest to the engineer involves burning of a hydrocarbon of fairly moderate volatility in air. For purposes of analysis by thermodynamic chart, an internal combustion engine cycle may be divided into (A) low temperature regions where chemical dissociation does not occur, or negligible in importance, and (B) high temperature regions, reached in combustion of the fuel, where chemical dissociation may become of appreciable magnitude.

Charts prepared by H. C. Hottel, G. C. Williams and C. N. Satterfield in 1949 (2), cover both the above regions for the gasoline engine cycle, and are satisfactory use with diesel engine cycles in region (A). They do not, however, cover the temperature range and pressure range of the diesel during combustion, i.e., in region (B).

The thermodynamic chart presented in this project covers the pressure and temperature range of the combustion portion of the diesel cycle for one typical diesel fuel-air ratio. It has been constructed on the same material and temperature bases as charts for gasoline engines in region (B), and thus may be used in conjunction with charts representing the unburned mixture, as prepared by Hottel, Williams and Satterfield (2). Values of equilibrium constants and thermodynamic property values used here are consistent with those used by Hottel, Williams and Satterfield (2).







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## CHAPTER II

### BASIC CONSIDERATIONS AND DATA

#### 1. Data Furnished by the Bureau of Ships

It was suggested by the Internal Combustion Engine Division of the Bureau of Ships that the thermodynamic chart be constructed for the following:

Fuel-Air Ratio = 0.5 (200% theoretical air).

Pressure Range: 800 p.s.i. to 1500 p.s.i.

Temperature Range: 3000° Rankine to 4500° Rankine.

#### 2. Chemical Dissociation

At the high temperatures reached in the combustion process of the diesel engine there may be many different molecular species present in varying amounts, due to chemical dissociation of the working fluid. The requirement of chemical equilibrium necessitates consideration of the effect of the species on the thermodynamic properties of the burned mixture. There are ten molecular species ( $N_2$ ,  $O_2$ ,  $CO_2$ ,  $H_2O$ ,  $NO$ ,  $OH$ ,  $CO$ ,  $O$ ,  $H_2$ , and  $H$ ) present in sufficient quantity to require consideration in this development. In the course of the project, it was found that the effect of the minor species ( $NO$ ,  $OH$ ,  $CO$ ,  $O$ ,  $H_2$ ,  $H$ ) was of definite importance in the temperature and pressure range involved. In Figure 1 is shown the effect of temperature on the relative magnitude of these species for one representative pressure. It is apparent that the magnitudes of these minor species become appreciable at the higher temperatures, and cannot be neglected with propriety. Particularly is this true of the species  $NO$  and  $OH$ , which frequently are



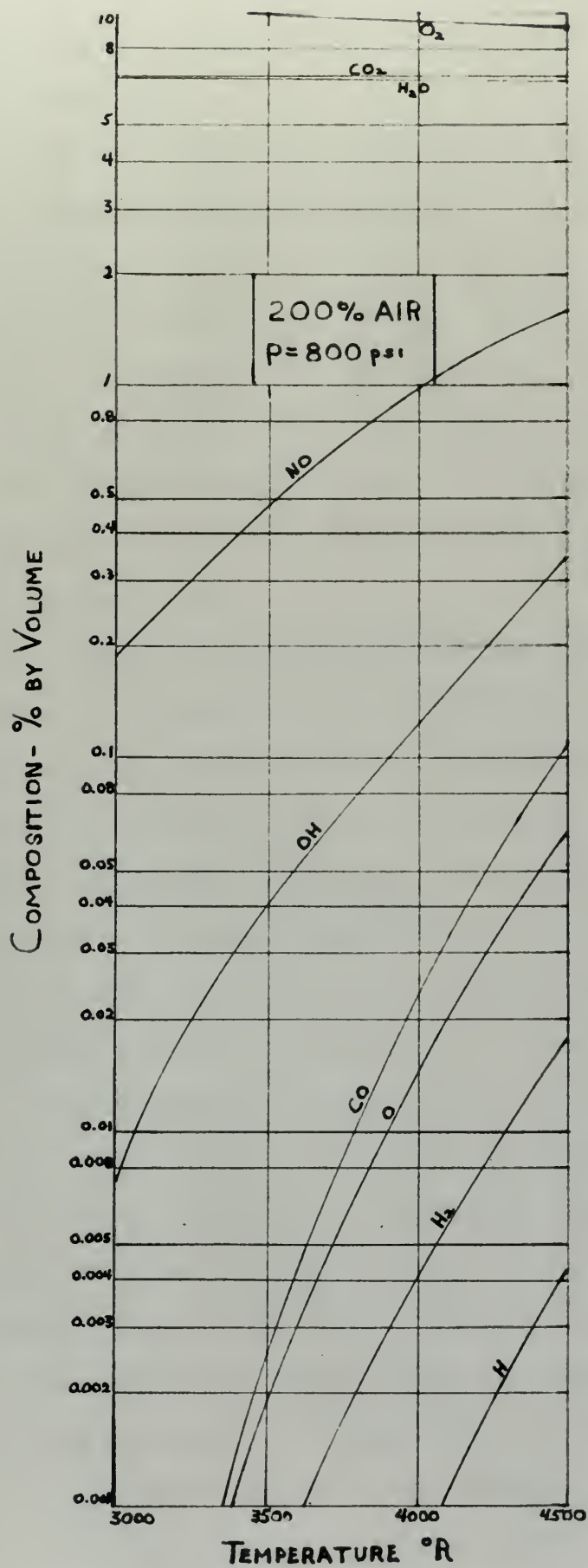


Fig. 1. Effect of Temperature on Magnitudes of Molecular Species.





neglected in determinations of burned mixture composition.

### 3. Ideal Gas Law

Computations involving composition of the burned mixture together with critical pressures and temperatures of the component species indicate that the burned mixture behaves as if its critical pressure and temperature are about 30.3 atmospheres and 320° Rankine, respectively. At the elevated temperatures of the chart deviations from the ideal gas law are insignificant. Therefore, the chart is based on the equation of state for ideal gases.

### 4. Fundamental Data

The fundamental data required for calculation of this chart are: (a) equilibrium constants as functions of temperature, and (b) various heats of reaction. The author has accepted for his calculations the same data on internal energies, enthalpies, entropies, and equilibrium constants as did Hottel, Williams and Satterfield (2). The method of determining the changes in the thermodynamic properties for the chemical reaction in question is given in Appendix I, page 16; the method of obtaining the actual equilibrium constants used in the calculation of composition of combustion products in equilibrium at the various temperatures and pressures is described briefly in Appendix I, page 14.

Composition of air: on a basis of 100 moles of dry air, a composition of 20.99 moles of oxygen and 79.01 moles of nitrogen was used. In actuality, the nitrogen above has minor components of argon carbon dioxide, and hydrogen included, and might better be termed Air-Nitrogen. The above





composition was used in calculating thermodynamic properties; but pure nitrogen was used in equilibrium calculations, which made but a negligible change in the amount of NO present.

Composition of fuel: the fuel chosen was the hydrocarbon  $(CH_2)_x$ , which has a hydrogen-carbon ratio considered adequately representative of diesel fuel.

Other constants:

1. Gas Constant R - 1.987 cal./°K. gram-mole.
2. Apparent Formula Mass of Air - 28.95 (which agrees with the above air composition.)
3. Atomic masses from 1936 International Tables.
4. Conversion Factor: 1 atmosphere - 14.696 p.s.i.
5. Conversion Factor: 1 cal./gram-mole - 1.80 BTU/lb.-mole.
6. Conversion Factor: 1 lb.-mole burned mixture - 0.0024135 pound of air.



## CHAPTER III

### PROCEDURE

#### 1. Analysis

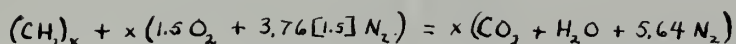
If definitely fixed quantities of carbon, hydrogen, oxygen and nitrogen are permitted to come into equilibrium, two of the properties of the resultant mixture may be fixed, and will be sufficient to completely define the composition of the mixture, and hence its thermodynamic properties. Pressure and temperature were the properties selected in this work.

It was considered that chemical dissociation would produce combustion products containing the following molecular species:  $N_2$ ,  $O_2$ ,  $CO_2$ ,  $H_2O$ ,  $CO$ ,  $H_2$ ,  $H$ ,  $OH$ ,  $O$  and  $NO$ . The relative magnitudes of these species, at the fixed fuel-air ratio, depend upon the pressure and temperature. The method used to calculate these magnitudes at a sample pressure and temperature, using determined data on equilibrium constants, is shown in Appendix II.

#### 2. Material Basis

The material basis of the chart is the quantity of material which contains nitrogen and oxygen equivalent to one pound of air.

For complete combustion:



For a fuel-air ratio of 0.5, there are three moles of oxygen and 11.280 moles of nitrogen, or 14.280 moles of air, for each  $CH_2$  unit of fuel. The mass of air is  $(14.280)(28.95)=$



413.406 pounds; the mass of fuel is  $(1)(12) + (2)(1.008) = 14.016$  pounds. The mass of fuel associated with one pound of air is then 0.033904 pounds. The mass basis is necessary for consistency because the number of moles of combustion products varies at elevated temperatures with variation of any thermodynamic property.

### 3. Determination of Thermodynamic Properties

The temperature base for the chart was selected as 100°F. The values of internal energy and entropy, obtained from Table 6, Appendix A, Hottel, Williams, and Satterfield, (2), were converted to this temperature base as described and illustrated in Appendix I. To determine the internal energy of the combustion products at each selected temperature and pressure, the procedure is to multiply the mole fraction of each molecular species in the products by its corresponding value of internal energy, corrected to proper temperature base, sum up these products for all ten species, and convert to the proper material basis for the chart; thus

$$E_{mix} = \sum x_i E_i$$

Entropy involves not only an additive factor similar to that shown above for internal energy, but also the entropy of mixing; that is, the entropy of the mixture is

$$S_{mix} = \sum (x_i S_i - x_i R \ln p_i)$$

where  $x_i$  is the mole fraction of each species,  $S_i$  is the molar entropy of each species at one atmosphere pressure





and each temperature, corrected to the proper temperature base,  $R$  is the gas constant, and  $P_i$  is the partial pressure of the components, in atmospheres, and also equals  $x_i P$ , where  $P$  is the total pressure of the mixture in atmospheres. The entropy  $S_{mix}$  is corrected to the proper material base for the chart. The enthalpy of the mixture is obtained from the thermodynamic relation

$$H_{mix} = E_{mix} + p V/J = E_{mix} + RT$$

The volume at each pressure and temperature is obtained from the ideal gas law:

$$V_{mix} = (\xi_m) R' T / 144 p$$

where  $(\xi_m)$  is the total moles of the mixture at each temperature and pressure,  $R'$  is the gas constant (1545 BTU/OR lb-mole) and  $p$  is the total pressure in pounds per square inch. This volume is then converted to the proper material basis of the chart.

#### 4. Description of Chart.

The thermodynamic properties represented on the chart are as follows:

(a) Temperature -  $T$ , degrees Rankine. Nearly horizontal solid lines at 200 degrees intervals.

(b) Pressure -  $p$ , pounds per square inch. Diagonal solid lines at 100 p.s.i. intervals.

(c) Volume -  $V$ , cubic feet per pound of original air. Diagonal dashed lines with greater slope than the pressure lines, at 0.1 or 0.2 cubic foot intervals.





(d) Internal Energy -  $E$ , BTU per pound of original air.  
Ordinate of chart.

(e) Entropy -  $S$ , BTU/°Rankine per pound of original air.  
Abscissa of chart.

(f) Enthalpy -  $H$ , BTU per pound of original air. Nearly horizontal dashed lines, superimposed on the chart to eliminate the necessity of using the relation  $H = E + RT$ .

#### 5. Method of Reading the Chart.

To illustrate reading the chart let it be desired to determine the thermodynamic properties of the products of combustion of one pound of air with  $(CH_2)_v$  vapor at  $T = 3600^\circ$  Rankine and  $p = 1200$  p.s.i. The original mixture contains <sup>150%</sup> 100% excess air. Locate the intersection of the lines corresponding to the above temperature and pressure, and read directly that the volume is 1.15 cubic feet; the internal energy is <sup>682</sup> 711.8 BTU; the enthalpy is <sup>94</sup> 953.2 BTU; and the entropy is <sup>264</sup> 0.285 BTU/° Rankine. Interpolation between temperature and enthalpy lines is substantially linear. In actual cycle analysis employing the chart, the known thermodynamic properties will be more probably be pressure and either internal energy or enthalpy, but the procedure in reading the chart remains the same.

#### 6. Use of Chart.

The chart is designed for use in conjunction with diagrams representative of the unburned mixture existing prior to combustion, in analyzing diesel cycles. Such diagrams have been prepared by Hottel, Williams, and Satterfield, (2). The author's chart indicates the thermodynamic properties of the burned mixture as a result of the combustion process.



## CHAPTER IV

### A DISCUSSION OF THE SYSTEM BELOW 3000° RANKINE

#### 1. Basic Requirements.

To permit determination of the thermodynamic properties of the burned mixture as a result of isentropic expansion to a point where the exhaust valve opens, a low pressure - low temperature chart, of substantially the same entropy limits as the author's chart, is required. The approximate temperature and pressure ranges for this chart are 900° Rankine to 2900° Rankine, and 14.7 p.s.i. to 190 p.s.i. respectively.

#### 2. Frozen Equilibria.

Chemical equilibrium has been assumed to exist at all temperatures above 3000° Rankine, where the chemical reaction velocity is quite high. However, when the gas mixture is rapidly cooled below 3000° Rankine, the composition is found to correspond to that at some higher temperature, at which the composition "froze". Considering that in diesel cycles an isentropic path is closest to the actual path to the system below 3000° Rankine, the pressure effect on composition was taken into account by the assumption that the composition of a mixture below 3000° Rankine was that of the mixture at 3000° Rankine, at the same entropy. Experimental validation of this assumption is quoted in Chapter V, Robinson (5), and is consistent, in this temperature and pressure range, with the value of 2880° Rankine, used by Hottel, Williams, and Satterfield (2).



### 3. Determination of Thermodynamic Properties.

The composition of the burned mixture at 3000° Rankine and at various pressures is determined as shown in Appendix B. The entropy of the mixture at 3000° Rankine and the above pressure is determined as described in paragraph 3 of Chapter III. As stated in paragraph 1 above, the composition of the burned mixture at any temperature below 3000° Rankine is that of the mixture at 3000° Rankine at the same entropy. Thus, selection of any temperature T in this region fixes two thermodynamic properties - temperature and entropy - and these are sufficient to define the remaining thermodynamic properties of the mixture. The internal energy and enthalpy at each temperature T is then obtained in the manner described in paragraph 3, Chapter III, using the mixture composition at 3000° Rankine at each entropy. To obtain pressure (p) and volume (V), the equations for the isentropic process by which this region is entered in the cycle, from the region above 3000° Rankine, are used. These are, at any temperature T and entropy S:

$$p = p_1 \left( \frac{T}{T_1} \right)^{k/k-1} \quad \text{and} \quad V = V_1 \left( \frac{T}{T_1} \right)^{1/k-1},$$

where  $p_1$ , and  $V_1$  are the pressure and volume at  $T_1 = 3000^\circ$  Rankine, and  $k$  is the mean specific heat ratio between the temperatures T and  $T_1$ . Values of the specific heat ratio for the  $(\text{CH}_2)_x$  fuel with 200% air, at any temperature between 300° Rankine and 4000° Rankine, may be found in Table 8, Gas Tables (3). The method of obtaining the mean specific heat ratio between any two temperatures, when the specific heat ratios at these limiting temperatures are known, is set forth in Kiefer, Stuart and Kinney (4).





## BIBLIOGRAPHY

1. Hersey, R. L., Eberhardt, J. E., and Hottel, H. C.,  
SAE Journal (Transactions) 39, 409 (1936)
2. Hottel, H. C., Williams, G. C., and Satterfield, C. N.,  
Thermodynamic Charts For Combustion Processes,  
John Wiley & Sons, Inc., New York, 1949
3. Keenan, J. H., and Kaye, J. Gas Tables. John Wiley &  
Sons, New York, 1948
4. Kiefer, P.J., Kinney, G. F., and Stuart, M. C.  
Engineering Thermodynamics, (Unpublished)
5. Robinson, C. S., The Thermodynamics of Firearms.  
McGraw-Hill Book Company, New York, 1943.





## APPENDIX I



TABLE I

Equilibrium Constants For Chemical Reactions

T,°R	K <sub>1</sub>	K <sub>2</sub>	K <sub>3</sub>	K <sub>4</sub>	K <sub>5</sub>	K <sub>6</sub>
3000	3.406	9.1658.10 <sup>-8</sup>	1.816.10 <sup>-10</sup>	3.981.10 <sup>-10</sup>	1.014.10 <sup>-4</sup>	5.053.10 <sup>-6</sup>
3600	4.782	5.777.10 <sup>-7</sup>	7.925.10 <sup>-8</sup>	2.037.10 <sup>-7</sup>	1.597.10 <sup>-3</sup>	1.627.10 <sup>-4</sup>
4500	6.435	3.512.10 <sup>-4</sup>	3.451.10 <sup>-5</sup>	9.122.10 <sup>-5</sup>	2.514.10 <sup>-2</sup>	5.232.10 <sup>-3</sup>

$$K_1 = \frac{P_{\infty} P_{H_2O}}{P_{CO_2} P_{H_2}}$$

$$K_4 = \frac{P_O P_{H_2}}{P_{H_2O}}$$

$$K_2 = \frac{P_{NO} P_{H_2}}{P_{H_2O} P_{N_2}^{1/2}}$$

$$K_5 = \frac{P_H}{P_{H_2}^{1/2}}$$

$$K_3 = \frac{P_{O_2} P_{H_2}^2}{P_{H_2O}^2}$$

$$K_6 = \frac{P_{OH} P_{H_2}^{1/2}}{P_{H_2O}}$$

$P_i$  in above is partial pressure in atmospheres, of each molecular species.

Equilibrium constants listed above were calculated from the series of values listed in Table 7, Appendix A, of Hottel, Williams, and Satterfield (2), by interpolation, employing the linear relationship between the reciprocal of absolute temperature (  $1/T_K$  ) and the natural logarithmic value of the equilibrium constant (  $\log_e K_n$  ).



TABLE II

## Thermodynamic Properties Of Molecular Species

Species	Internal Energy				Enthalpy			
	3000°	3600°	4500°	3000°	3600°	4500°	H	
CO <sub>2</sub>	14326	18448	24898	17638	22422	29866		
H <sub>2</sub> O	10659	13979	19301	13971	17953	24269		
Air-N <sub>2</sub>	7765	9992	13266	11077	13966	18234		
O <sub>2</sub>	8395	10712	14301	11709	14686	19269		
CO	75265	77467	80846	78577	81441	85814		
H <sub>2</sub>	64718	66733	69925	68030	70707	74893		
H	84601	85594	87085	87913	89568	92053		
OH	45423	47473	50721	48735	51447	55689		
NO	29696	31928	35349	33008	35902	40317		
O	62799	63792	65283	66111	67766	70251		

The units of the above are calories/g-mole.

The values shown above were obtained from those in Table 6, Appendix A, Hottel, Williams, and Satterfield (2), in the following manner, using the internal energy of species CO at  $T = 3600^\circ$  as an example.



The internal energy of any species at temperature  $T$  equals  $E_s + Q_v$  where  $E_s$  is the heat released by cooling the gas at constant volume to the temperature base of the chart ( $100^\circ\text{F} = 311^\circ\text{K}$ ), and  $Q_v$  is the heat of combustion of the gas at constant volume at  $100^\circ\text{F}$ .  $E_s$  is the value of  $E$  of the species at temperature  $T$  minus the value of  $E$  of the species at  $100^\circ\text{F}$ , each obtained from Table 6, Appendix A, Hottel, Williams, and Satterfield (2).  $Q_v$  at  $100^\circ\text{F}$  is the heat evolved in cooling the species, and oxygen required for combustion, down to  $0^\circ\text{K}$ , plus the heat of combustion at  $0^\circ\text{K}$  ( $E$  at  $0^\circ\text{K}$  in Table 6), less the heat absorbed in heating the combustion products from  $0^\circ\text{K}$  to  $311^\circ\text{K}$  ( $100^\circ\text{F}$ ).

For the combustion of  $\text{CO}$ , the combustion equation is:



or one mole of species  $\text{CO}$  reacts with one half mole of oxygen to form one mole of  $\text{CO}_2$  as combustion products. From Table 6, Appendix A, Hottel, Williams, and Satterfield (2), the following values are obtained:

For $\text{CO}$ :	$E_{0^\circ\text{K}} = 66,769$	For $\text{CO}_2$ :	$E_{311^\circ\text{K}} - E_{0^\circ\text{K}} = 1737$
	$E_{311^\circ\text{K}} = 73,757$	For $\text{O}_2$ :	$E_{311^\circ\text{K}} - E_{0^\circ\text{K}} = 1538$
	$E_{3600^\circ\text{R}} = 78,435$		

Then:

$$E_s = E_{3600^\circ\text{R}} - E_{311^\circ\text{K}} = 78435 - 73757 = 4678$$

$$Q_v = [E_{311^\circ\text{K}} - E_{0^\circ\text{K}}]_{\text{CO}} + [E_{311^\circ\text{K}} - E_{0^\circ\text{K}}]_{\text{O}_2} \times \frac{1}{2} + [E_{0^\circ\text{K}}]_{\text{CO}} - [E_{311^\circ\text{K}} - E_{0^\circ\text{K}}]_{\text{CO}_2}$$





$$Q_v = (73757 - 66769) + \frac{1538}{2} + 66769 - 1737$$

$$= 72789$$

$$E_{3600^{\circ}\text{R}} = E_s + Q_v$$

$$= 4678 + 72789 = 77467 \text{ calories/g-mole.}$$

The above is the value shown in Table 2.

The value of enthalpy is readily obtained from the relation  $H = E + RT$ . Thus the enthalpy of CO at  $T = 3600^{\circ}\text{R}$  is:

$$H_{3600^{\circ}\text{R}} = E_{3600^{\circ}\text{R}} + 1.987 \times 2000$$

$$= 77467 + 3974 = 81441 \text{ calories/g-mole}$$

TABLE III

Molar Entropy (at one atmosphere pressure)

Species	$T = 3000^{\circ}\text{R}$	$T = 3600^{\circ}\text{R}$	$T = 4500^{\circ}\text{R}$
CO <sub>2</sub>	20.166	22.522	25.791
H <sub>2</sub> O	15.910	17.875	20.68
Air-N <sub>2</sub>	12.754	14.148	16.072
O <sub>2</sub>	13.490	14.956	16.993
CO	12.924	14.336	16.279
H <sub>2</sub>	12.061	13.537	15.397
H	8.34	9.26	10.36
OH	12.40	13.74	15.62
NO	13.21	14.65	16.61
O	8.34	9.26	10.36

The units of the above are calories/g-mole<sup>°K</sup>, or BTU/lb-mole<sup>°R</sup>.



The values shown in the preceding table (Table III) were obtained from those in Table 6, Appendix A, Hottel, Williams, and Satterfield (2), merely by subtracting the entropy value at the temperature base of the chart ( $100^{\circ}\text{F} = 311^{\circ}\text{K}$ ) from the entropy corresponding to the temperature in question.

TABLE IV

Thermodynamic Properties of Equilibrium Mixture of Combustion Products From Which Chart Was Constructed:

T	P	E	H	S	V
$^{\circ}\text{R}$	psi	BTU	BTU	BTU/ $^{\circ}\text{R}$	cu.ft.
3000	800	548.376	761.731	0.25860	1.4399
3000	1200	548.356	761.711	0.22988	0.9599
3000	1500	548.347	761.701	0.21385	0.7680
3600	800	711.951	953.289	0.31384	1.7281
3600	1000	711.855	953.191	0.29724	1.3825
3600	1200	711.777	953.110	0.28499	1.1521
3600	1400	711.720	953.052	0.27403	0.9875
3600	1500	711.687	953.017	0.26909	0.9216
4500	800	976.566	1297.191	0.39238	2.1633
4500	1200	974.417	1294.959	0.36334	1.4422
4500	1500	973.242	1293.749	0.34733	1.1536

The material basis consistent with the above values is one pound of dry air ( $1/28.95$  pound-mole), plus the corresponding fuel.



## APPENDIX II



# Method Of Calculating Composition Of Combustion Products In Equilibrium

The large number of molecular species present in the combustion equilibrium mixture makes it necessary to organize the method of calculation to minimize trial-and-error.

There are four kinds of atoms present (C, H, O, N). These are distributed in ten species ( $\text{CO}_2$ ,  $\text{H}_2\text{O}$ ,  $\text{O}_2$ ,  $\text{N}_2$ ,  $\text{CO}$ ,  $\text{H}_2$ ,  $\text{H}$ ,  $\text{OH}$ ,  $\text{NO}$ ,  $\text{O}$ ). Available in relating these species are the six chemical equilibrium equations shown in Table I, Appendix I. They are listed again here for convenient reference, with the number of moles of each species being represented by its chemical symbol in parenthesis:

$$E_{q. 1} \quad K_1 = P_{\text{CO}} P_{\text{H}_2\text{O}} / P_{\text{CO}_2} P_{\text{H}_2} = (\text{CO})(\text{H}_2\text{O}) / (\text{CO}_2)(\text{H}_2)$$

$$E_{q. 2} \quad K_2 = P_{\text{NO}} P_{\text{H}_2} / P_{\text{H}_2\text{O}} P_{\text{N}_2}^{1/2} = (\text{NO})(\text{H}_2) / (\text{H}_2\text{O})(\text{N}_2)^{1/2} \times \sqrt{P/\xi}$$

$$E_{q. 3} \quad K_3 = P_{\text{O}_2} P_{\text{H}_2}^2 / P_{\text{H}_2\text{O}}^2 = (\text{O})(\text{H}_2)^2 / (\text{H}_2\text{O})^2 \times P/\xi$$

$$E_{q. 4} \quad K_4 = P_{\text{O}} P_{\text{H}_2} / P_{\text{H}_2\text{O}} = (\text{O})(\text{H}_2) / (\text{H}_2\text{O}) \times P/\xi$$

$$E_{q. 5} \quad K_5 = P_{\text{H}} / P_{\text{H}_2}^{1/2} = (\text{H}) / (\text{H}_2)^{1/2} \times \sqrt{P/\xi}$$

$$E_{q. 6} \quad K_6 = P_{\text{OH}} P_{\text{H}_2}^{1/2} / P_{\text{H}_2\text{O}} = (\text{OH})(\text{H}_2)^{1/2} / (\text{H}_2\text{O}) \times \sqrt{P/\xi}$$

In the above,  $P$  is the total pressure in atmospheres,  $P_i$  is the partial pressure in atmospheres of each molecular species, and the symbol  $\xi$  represents the sum of the moles of all species present.





As shown in Chapter III (4), with a fuel-air ratio of 0.5, or 200% air, there are 3 moles of  $O_2$  and 3.76(3) 11.280 moles of  $N_2$  present, giving 14.280 moles of air per mole of fuel. If one mole of carbon and of hydrogen in the fuel is chosen as a basis, there are available the following four equations satisfying the material balance of the four atoms present (C, H, O, N). These equations are, on a mole basis, at equilibrium:

$$Eq. 7. \quad (CO_2) + (CO) = 1.000$$

$$Eq. 8. \quad (H_2O) + (H_2) + \frac{1}{2} [(H) + (OH)] = 1.000$$

$$Eq. 9. \quad (CO_2) + (O_2) + \frac{1}{2} [(H_2O) + (CO) + (OH) + (NO) + (O)] = 3.000$$

$$Eq. 10. \quad (N_2) + \frac{1}{2} (NO) = 11.280$$

The equations 1 to 10 inclusive give sufficient relations to solve for the composition of the ten molecular species in the combustion products.

Procedure: The first step is to divide the ten species into major components ( $CO_2$ ,  $H_2O$ ,  $O_2$ ,  $N_2$ ,  $CO$  and  $H_2$ ), and minor components ( $H$ ,  $O$ ,  $NO$ , and  $OH$ ) and to consider for the first approximation of composition that only major components are present. Then equations 7 to 10 inclusive become

$$Eq. 7A. \quad (CO_2) + (CO) = 1.000$$

$$Eq. 8A. \quad (H_2O) + (H_2) = 1.000$$

$$Eq. 9A. \quad (CO_2) + (O_2) + \frac{1}{2} [(H_2O) + (CO)] = 3.000$$



$$\text{Eq. 10A.} \quad (N_2) = 11.280 \quad \text{and}$$

$$\text{Eq. 11.} \quad \sum = (\text{CO}_2) + (\text{H}_2\text{O}) + (\text{O}_2) + (\text{N}_2) + (\text{CO}) + (\text{H}_2)$$

By judicious use of the above five equations together with equations 1 and 3, a first approximation of the number of moles of the major species present may be obtained. Then, using these results, plus equations 2, 4, 5 and 6, a first approximation of the minor species is made. The values of the minor species so obtained are put into the original four equations 7, 8, 9, 10 and these equations in turn solved in terms of the major species. A second approximation is now carried out, in precisely the same manner as the first approximation, to give corrected values of the major species based upon the presence of minor species. Again values of the minor species are determined with the aid of equations 2, 4, 5 and 6. If the results for all species now satisfy equations 7, 8, 9, and 10 the computation is completed; if not, further approximations are carried through until these equations are perfectly satisfied.

To illustrate the method, a sample calculation will be performed, using representative values of temperature and pressure.

$$\text{Let } T = 3000^\circ\text{R} \quad \text{Let } p = 800 \text{ p.s.i., } P = 54.4 \text{ atmospheres}$$

From Table I, Appendix I, at  $T = 3000^\circ\text{R}$ :

$K_1 = 3.406$	$K_4 = 3.981 \cdot 10^{-10}$
$K_2 = 9.165 \cdot 10^{-8}$	$K_5 = 1.014 \cdot 10^{-4}$
$K_3 = 1.816 \cdot 10^{-10}$	$K_6 = 5.053 \cdot 10^{-6}$



$$E_{q. 1.} \quad \frac{(CO)(H_2O)}{(CO_2)(H_2)} = K_1 = 3.406$$

$$E_{q. 3.} \quad \frac{(O_2)(H_2)^2}{(H_2O)^2} = K_3 \left[ \frac{\sum}{P} \right] = 1.816 \cdot 10^{-10} \left[ \frac{\sum}{P} \right]$$

or

$$\frac{(H_2)}{(H_2O)} = 1.347 \cdot 10^{-5} \left[ \sqrt{\frac{\sum}{P(O_2)}} \right]$$

Adding equations 7A, 8A and 10A:

$$E_{q. 12.} \quad (CO_2) + (CO) + (H_2O) + (H_2) + (N_2) = 13.280 \quad \text{and}$$

$$E_{q. 13.} \quad \sum = 13.280 + (O_2)$$

Multiplying equation 9A by two and subtracting equation 7A:

$$E_{q. 14.} \quad (CO_2) + (H_2O) + 2(O_2) = 5.000$$

From equation 10A,  $(N_2) = 11.280$

#### 1ST APPROXIMATION

		<u>1.</u>	<u>2.</u>	
$(O_2)$		1.50061	1.5000127	$(O_2)$
$\sum = 13.280 + (O_2)$	$[E_{q. 13}]$	14.78061	14.7800127	
$\sqrt{\frac{\sum}{P(O_2)}}$		0.428	0.428	
$(H_2)/(H_2O) = 1.347 \cdot 10^{-5} \sqrt{\frac{\sum}{P(O_2)}}$	$[E_{q. 3}]$	$0.575 \cdot 10^{-5}$	$0.575 \cdot 10^{-5}$	
$(H_2)$		0.00000575	0.00000575	$(H_2)$
$(H_2O) = 1.000 - (H_2)$	$[E_{q. 8A}]$	0.99999425	0.99999425	$(H_2O)$
$(CO_2) = 5.000 - 2(O_2) - (H_2O)$	$[E_{q. 14}]$	0.99878575	0.9999804	$(CO_2)$
$(CO) = 1.000 - (CO_2)$	$[E_{q. 7A}]$	0.00121425	0.0000196	$(CO)$
$(CO)(H_2O)/(CO_2)(H_2) = 3.406$	$[E_{q. 1}]$	—	3.406	



$$\begin{aligned}
 \text{Eq. 5.} \quad (H) &= (K_5) \cdot (H_2)^{1/2} \cdot \sqrt{\frac{\xi}{P}} \\
 &= (1.014 \cdot 10^{-8}) (0.00000575)^{1/2} \left( \frac{14.7800127}{54.4} \right)^{1/2} \\
 &= 0.000001266
 \end{aligned}$$

$$\begin{aligned}
 \text{Eq. 6.} \quad (OH) &= (K_6) \cdot \frac{(H_2O)}{(H_2)^{1/2}} \cdot \sqrt{\frac{\xi}{P}} \\
 &= (5.053 \cdot 10^{-6}) \cdot \frac{(0.99999425)}{(0.00000575)^{1/2}} \cdot \left( \frac{14.7800127}{54.4} \right)^{1/2} \\
 &= 0.001100
 \end{aligned}$$

$$\begin{aligned}
 \text{Eq. 2} \quad (NO) &= (K_2) \cdot \frac{(H_2O)}{(H_2)} \cdot (N_2)^{1/2} \cdot \sqrt{\frac{\xi}{P}} \\
 &= (9.165 \cdot 10^{-8}) \cdot \frac{(0.99999425)}{(0.00000575)} \cdot (11.280)^{1/2} \cdot \left( \frac{14.7800127}{54.4} \right)^{1/2} \\
 &= 0.0280
 \end{aligned}$$

$$\begin{aligned}
 \text{Eq. 4} \quad (O) &= (K_4) \cdot \frac{(H_2O)}{(H_2)} \cdot \frac{\xi}{P} \\
 &= (3.981 \cdot 10^{-10}) \cdot \frac{(0.99999425)}{(0.00000575)} \cdot \left( \frac{14.7800127}{54.4} \right) \\
 &= 0.00001872
 \end{aligned}$$

Substituting these values for the minor species in equations 7, 8, 9, 10:

$$\text{Eq. 7} \quad (CO_2) + (CO) = 1.000$$

$$\begin{aligned}
 \text{Eq. 8} \quad (H_2O) + (H_2) &= 1.000 - \frac{1}{2} [(H) + (OH)] \\
 &= 0.99944937
 \end{aligned}$$

$$\begin{aligned}
 \text{Eq. 9} \quad (CO_2) + (O_2) + \frac{1}{2} [(H_2O) + (CO)] &= 3.000 - \frac{1}{2} [(OH) + (NO) + (O)] \\
 &= 2.985441
 \end{aligned}$$







$$\begin{aligned} \text{Eq. 10} \quad (N_2) &= 11.280 - \frac{1}{2} (NO) \\ &= 11.266 \end{aligned}$$

Now, following the same procedure as before:

Adding Eq. 7, 8, and 10;

$$\text{Eq. 12A} \quad (CO_2) + (CO) + (H_2O) + (H_2) + (N_2) = 13.2654494 \quad \text{and}$$

$$\text{Eq. 13A} \quad \Sigma = 13.2654494 + (O_2)$$

Multiplying Eq. 9 by two and subtracting Eq. 7:

$$\text{Eq. 14A} \quad (CO_2) + (H_2O) + 2(O_2) = 4.970882$$

## 2ND APPROXIMATION

$(O_2)$		1.49001	1.485729	$(O_2)$
$\Sigma = 13.2654494 + (O_2)$	[Eq. 13A]	14.75546	14.751178	
$\sqrt{\frac{\Sigma}{P(O_2)}}$		0.427	0.428	
$(H_2)/(H_2O) = 1.347 \cdot 10^5 \sqrt{\frac{\Sigma}{P(O_2)}}$	[Eq. 3]	$0.575 \cdot 10^{-5}$	$0.575 \cdot 10^{-5}$	
$(H_2)$		0.00000575	0.00000575	$(H_2)$
$(H_2O) = 0.99944937 - (H_2)$	[Eq. 8]	0.99944362	0.99944362	$(H_2O)$
$(CO_2) = 4.970882 - 2(O_2) - (H_2O)$	[Eq. 14A]	0.9914184	0.9999804	$(CO_2)$
$(CO) = 1.000 - (CO_2)$	[Eq. 7]	0.0085816	0.0000196	$(CO)$
$(CO)(H_2O)/(CO_2)(H_2) = 3.406$	[Eq. 1]		3.406	



Again determining the minor species from Eqs. 5, 6, 2 and 4:

$$(H) = 0.000001266$$

$$(OH) = 0.001100$$

$$(NO) = 0.02800$$

$$(O) = 0.00001872$$

The values of these species have not changed from those obtained in the first approximation, and hence all values satisfy equations 7, 8, 9, and 10; if they had not, a third approximation would have been required, performed in the same manner as the above.

Final Results:

$$(CO_2) = 0.9999804$$

$$(H_2O) = 0.99944362$$

$$(O_2) = 1.485729$$

$$(N_2) = 11.266$$

$$(CO) = 0.0000196$$

$$(H_2) = 0.00000575$$

$$(H) = 0.000001266$$

$$(OH) = 0.001100$$

$$(NO) = 0.02800$$

$$(O) = 0.00001872$$

$$\Sigma = 13.74019836$$



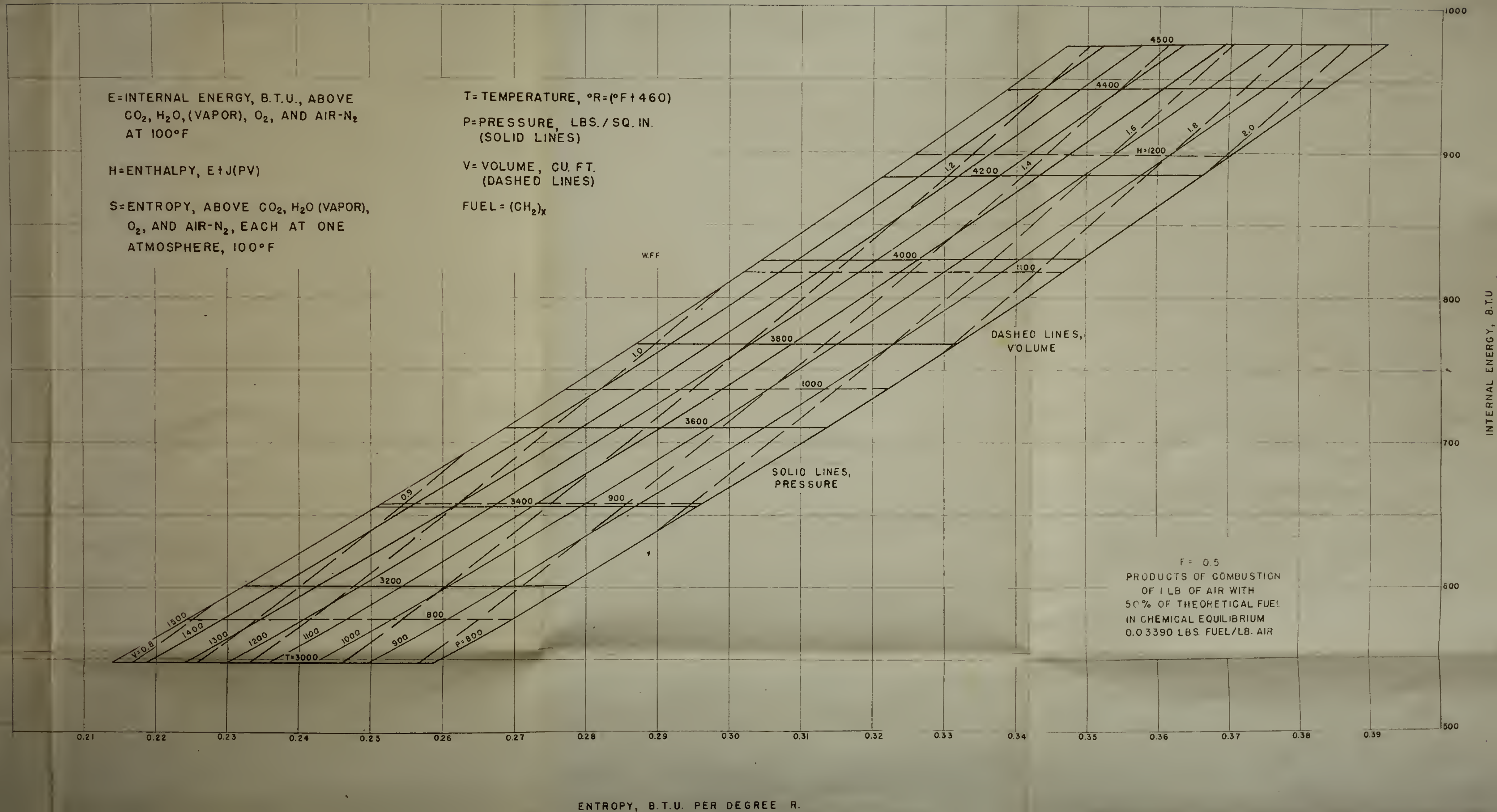












Thesis

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A thermodynamic chart  
for the combustion  
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A thermodynamic chart for the combustion



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